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1 Short Communication

2 Efficient production of biolipids by crude glycerol-assimilating fungi

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16

18 Abstract

19 The aim of this study was to isolate microorganisms utilizing crude glycerol as a carbon 20 source efficiently and to evaluate their lipid productivity. Fusarium oxysporum W1 grew 21 well on medium containing 20% crude glycerol as well as 50% pure glycerol. The dry cell 22 weights and total fatty acids of F. oxysporum W1 reached 24.5 g/L and 12.4 g/L. 23 Penicillium sp. N1 and P. citrinum N3 were found to accumulate free fatty acids to as much 24 as 56.2 % and 48.5 % of total fatty acids, respectively, on cultivation in the crude 25 glycerol-containing medium. These strains grew well on medium containing crude glycerol 26 only heat-treated at 80-105°C without autoclave sterilization.

27

28 Key words

29 Crude glycerol; Biolipid; Penicillium; Fusarium

30

31 1. Introduction

32 Biodiesel, a mixture of long-chain mono-alkyl fatty acid esters derived from vegetable oils or animal fats, as an alternative to petroleum, has attracted increasing attention in 33 34 recent years. The predominant process in biodiesel production is a transesterification phase, 35 which consists of a chemical reaction between lipids and an alcohol (methanol or ethanol) 36 in the presence of an alkali catalyst (Leoneti et al., 2012). However, this reaction also yields 37 approximately 1 kg of crude glycerol, which comprises not only glycerol but also soap, 38 salts, methanol, alkaline catalyst residues, and plant-derived organic matter, for every 10 kg 39 of biodiesel production (Johnson and Taconi, 2007; Thompson and He, 2006). The increase 40 in crude glycerol emissions resulting from the increase in biodiesel production is a serious 41 problem for the biodiesel industry, and is a financial and environmental responsibility.

42 The purification process for crude glycerol involving nanoparticle, enzyme catalytic 43 system, supercritical, and membrane filtration methods yields pure glycerol (Wan Isahak et 44 al., 2015; Ilham and Saka, 2016; Chol et al., 2018), but its attractiveness has been reduced 45 in terms of high purification costs. Therefore, fermentation systems in which oleaginous 46 microorganisms such as Aurantiochytrium sp., Yarrowia lipolytica, Rhodotorula sp., and 47 *Cryptococcus* sp. produce biolipids with crude glycerol as a carbon source are becoming 48 promising (Chang et al., 2015; Gao et al., 2016; Polburee et al., 2015; Poli et al., 2014). To 49 use crude glycerol efficiently for fermentation, it is desirable to isolate microorganism 50 strains exhibiting excellent glycerol utilization. We evaluated the lipid productivity of 51 bacteria, yeast, and filamentous fungi growing in a medium containing crude glycerol. Here, 52 we isolated three filamentous fungi that are superior in growth and lipid productivity on 53 cultivation with high concentrations of pure glycerol as a carbon source. Furthermore, these 54 strains grew well in a medium containing crude glycerol as a carbon source. They are 55 expected to be useful breeding stocks for the biolipids production process involving pure 56 and crude glycerol.

57

58 **2. Materials and methods**

59 2.1. Materials

60 Unrefined crude glycerol, which contains approximately 45% (w/w) glycerol, 13% 61 (w/w) lipids/soap, 13% (w/w) methanol, 2.7% (w/w) potassium and other impurities, was 62 obtained from the Kyoto Municipal Waste Edible Oil Fuel Production Facility, Japan. Pure 63 glycerol and yeast extract were purchased from Nacalai Tesque Inc. (Japan) and Oriental 64 Yeast Co., Ltd. (Japan), respectively.

66	2.2. Isolation and identification of highly concentrated pure glycerol-assimilating fungi					
67	Various soil and sewage samples were collected in Tokushima, Japan. The samples					
68	were streaked on to selection plates [20% (w/v) pure glycerol, 0.5% (w/v) yeast extract and					
69	1% (w/v) agar] and then incubated at 28°C. Strains appearing on the plates were isolated					
70	and then cultivated in a medium containing 50% (w/v) pure glycerol and 0.5% (w/v) yeast					
71	extract at 28°C and 300 rpm for 7 days.					
72	The strains isolated were identified by sequencing of the internal transcribed spacer and					
73	5.8S ribosomal DNA region (ITS-5.8S rDNA) amplified with pair of primers; ITS1:					
74	5'-TCCGTAGGTGAACCTGCGG-3' and ITS4: 5'-TCCTCCGCTTATTGATATGC-3'					
75	(White et al., 1990). The amplified PCR products were sequenced (Macrogen Inc., Kyoto,					
76	Japan) and analyzed using the BLASTn algorithm of the National Center for Biotechnology					
77	Information (NCBI, <u>http://blast.ncbi.nlm.nih.gov/</u>).					
78						
79	2.3. Culture conditions					
80	Crude glycerol medium, named CG medium, that contained 2-30% (w/v) crude glycerol					
81	and 1% (w/v) yeast extract was used for microbial cultivation. CG medium containing 10%					
82	crude glycerol included 4.5% glycerol component. To evaluate the effect of heat treatment					
83	of CG medium on microbial cultivation, CG medium containing 4% crude glycerol was					
84	treated at 40, 50, 60, 70, 80, 90, 105, or 110°C for 30 min or 1 h without autoclave					
85	sterilization. All strains were cultivated in the CG medium prepared with reciprocal shaking					
86	at 300 rpm and 28°C for 7 days and analyzed as to their fatty acid productivities.					

88 2.4. Fatty acid analysis

89 Mycelial cells were harvested by suction filtration, washed with distilled water, and 90 then dried at 110°C for 3 h. The dried cells were transmethylated with 10% methanolic HCl 91 (acetyl chloride: methanol = 1:9, v:v) and dichloromethane at 55° C for 2 h. The resultant 92 fatty acid methyl esters were extracted with *n*-hexane, concentrated, and then analyzed by 93 gas chromatography (GC) as described previously (Okuda et al., 2015). Tricosanoic acid 94 (23:0) was used as an internal standard. Mycelial total lipids were extracted with the 95 chloroform/methanol/water system described by Bligh and Dyer (1959). To separate lipid 96 classes, extracted total lipids were spotted on to thin-layer chromatography Silica Gel 60 97 F254 plates (Merck KGaA, Germany) and then developed with hexane/diethyl ether/acetic 98 acid (80:20:1, v:v:v). The lipid classes were visualized with a primulin solution [0.001% 99 (w/v) primulin in an acetone-water solution (4:1, v:v)] and analyzed by GC, as described 100 above.

101

102 **3. Results and discussion**

103 3.1. Crude glycerol tolerance and fatty acid productivity of the isolated strains

In this study, we obtained three filamentous fungi, *Penicillium* sp. N1, *P. citrinum* N3, and *Fusarium oxysporum* W1, which were cultured in medium containing 50% pure glycerol. These strains showed 21-33 g/L of lipid productivity in medium containing 10% pure glycerol. Compared to oleaginous fungus *Mortierella alpina* CBS754.68, three strains isolated in this study exhibited higher growth and lipid productivity on the medium containing high concentrations of pure glycerol. Strains N1 and N3 grew well in CG 110 medium containing 10% crude glycerol and their dry cell weights (DCW) had reached 41.0 111 g/L and 29.7 g/L, respectively, on the 7th day (Fig. 1). The growth of strains N1 and N3 112 was poor in the CG medium containing 20% or more crude glycerol (Fig. 1). On the other 113 hand, the DCW of strain W1 reached the highest value of 24.5 g/L on cultivation in the CG 114 medium containing 20% crude glycerol (Fig. 1). These results indicated that strain W1 is 115 more resistant to crude glycerol than strains N1 and N3. In particular, the weight of the total 116 fatty acids in strain W1 accounted for about 50% of its DCW (Fig. 1). The lipid 117 productivity of three strains was higher when they were cultivated in CG medium (Fig. 1) 118 than in pure glycerol medium, suggesting that these three strains efficiently took up lipids 119 contained in crude glycerol into their cells.

120 Crude glycerol, which contains some impurities such as methanol, soap, and alkali 121 catalysts, was reported to inhibit the growth of microorganisms and bioconversion into 122 value-added products (Ardi et al., 2015). Studies on the fermentation process using 2-8% 123 crude glycerol with low methanol and soap content as a carbon source have been reported 124 so far (Chatzifragkou et al., 2011; Liang et al., 2010; Tang et al., 2009). On the other hand, 125 in the oleaginous yeast *Rhodosporidium toruloides* 32489, the lipid production by using 126 crude glycerol was higher than that by using glucose or pure glycerol (Gao et al., 2016). 127 Among the impurities in crude glycerol, methyl oleate, sodium oleate, and NaCl had a 128 promoting effect in this yeast, while only methanol had an inhibitory effect (Gao et al., 129 2016). The crude glycerol sample used in this study contained more impurities as described 130 above. Strain W1 isolated in this study, which grew in the CG medium containing 20% 131 crude glycerol, is expected to be one of promising producers of microbial lipids.

132



133

Fig. 1. The effects of crude glycerol on fatty acid production and fugal growth. Thestrains were cultivated in CG medium containing 2 to 30% crude glycerol for 7 days.

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3.2. Analysis of fatty acid composition in each lipid class from mycelia cultivated in the CGmedium

Quantitative analysis of lipid classes by TLC and GC revealed that the major lipid class in strains N1 and N3 cultured in the CG medium was free fatty acid (FFA) (Table 1). Fatty acid methyl ester (FAME) accounted for about 3% of the total lipids in strains N1 and N3. The crude glycerol used in this study contained about 13% (w/w) lipids/soap, in which FFA and FAME accounted for about 81% (w/w) and 18% (w/w), respectively (Table 1). These 145 results suggested that strains N1 and N3 accumulated FFAs and FAMEs derived from the 146 crude glycerol in their mycelia. However, while the percentage of linoleic acid (18:206) in 147 the FFA fraction of crude glycerol was 27.73%, the FFA of strains N1 and N3 contained 148 7.74% and 6.53% of linoleic acid, respectively. Strains N1 and N3 accumulated about 20% 149 FFAs in total lipids on cultivation in the medium containing pure glycerol as a carbon 150 source (data not shown). FFAs induce cell death (lipotoxicity) and the inductive effect 151 depends on the length of the carbon chain and the number of double bonds (Maia et al. 152 2010; Desbois and Smith 2010). In strains N1 and N3, the FFAs of linoleic and α -linolenic 153 acid (18:3 ω 3), which are considered to be more toxic for mycelia, may have been 154 selectively converted to acylglycerols such as diacylglycerols (DAGs) and triacylglycerols 155 (TAGs) or metabolized via β-oxidation. Penicillium spp. N1 and N3 accumulated FFAs 156 containing about 70% oleic acid (18:109) in their mycelia. Penicillium spp. are known to 157 have useful lipases and to produce fatty acids with grease waste as a substrate (Gutarra et 158 al., 2009; Kumari et al., 2017; Lima et al., 2019). We first found in this study that 159 Penicillium spp. N1 and N3 have high ability to accumulate FFAs.

The lipid composition in *F. oxysporum* W1, which included 96.98% TAG and 0.94% FFA, differed from those in *Penicillium* spp. N1 and N3 (Table 1). These results suggested that strain W1 utilized fatty acids derived from the crude glycerol for TAG synthesis as well as the crude glycerol as a carbon source. Generally, FFA is converted to acyl-CoA by acyl-CoA synthase and then bound to phospholipid, monoacylglycerol and diacylglycerol by acyltransferases. Strain W1 is expected to have high ability for lipid construction.

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D:	Lipid	Fatty acid content	Relative fatty acid composition (%) ^b							
Derivation	class ^a	(% of TFA)	16:0	18:0	18:1w9	18:2w6	18:3w3	20:0	22:0	Others
N1	PL	3.04	13.21	3.81	48.44	29.43	2.05	1.07	0.53	1.46
	DAG	2.96	6.44	3.32	51.32	36.07	2.24	0.32	0.11	0.19
	FFA	56.19	3.19	12.07	69.77	7.74	2.29	3.26	1.22	0.47
	TAG	34.04	4.96	1.25	50.38	40.89	2.19	0.20	0.04	0.10
	FAME	3.43	4.89	6.22	67.27	11.78	2.07	2.84	2.99	1.93
	SE	0.34	22.45	27.06	39.52	7.52	1.67	0.74	0.73	0.31
N3	PL	2.29	15.37	5.59	47.13	25.87	2.30	1.17	0.78	1.80
	DAG	2.67	7.85	3.55	45.40	39.57	2.94	0.26	0.11	0.32
	FFA	48.52	3.68	12.04	70.94	6.53	2.21	3.00	1.15	0.45
	TAG	43.04	5.95	1.04	45.23	44.59	2.93	0.12	0.02	0.10
	FAME	3.20	7.47	7.88	60.73	15.53	1.66	2.15	2.93	1.65
	SE	0.28	27.30	28.55	31.04	10.01	1.41	0.49	0.63	0.58
W1	PL	1.34	16.33	2.90	18.92	59.52	1.72	0.06	0.09	0.46
	DAG	0.73	13.97	7.36	34.75	40.10	3.01	0.08	0.30	0.43
	FFA	0.94	15.91	9.35	27.96	20.17	9.52	0.21	12.11	4.77
	TAG	96.98	7.79	3.55	44.50	38.83	4.87	0.05	0.12	0.30
	FAME	n.d. ^c	d	—	_	_	—	_	_	—
	SE	n.d.	—	—	_	_	_	_	—	_
Crude Glycerol	PL	1.19	68.81	31.19	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
	DAG	n.d.	_	_	_	_	_	_	_	—
	FFA	81.05	11.50	3.97	52.25	27.73	4.54	n.d.	n.d.	n.d.
	TAG	n.d.	_	_	_	_	_	_	_	_
	FAME	17.75	18.57	5.61	49.74	23.00	3.09	n.d.	n.d.	n.d.
	SE	n.d.	_	_	_	—	—	—	—	_

Table 1. Lipid class and fatty acid composition. The strains were cultivated in CG medium containing 10% crude glycerol.

^a Abbreviations: PL, polar lipid; DGA, diacylglycerol; FFA, free fatty acid; TAG,

169 triacylglycerol; FAME, fatty acid methyl ester; SE, sterol ester.

^b Abbreviations: 16:0, palmitic acid; 18:0, stearic acid; 18:1ω9, oleic acid; 18:2ω6, linoleic

171 acid; $18:3\omega 3$, α -linolenic acid; 20:0, arachidic acid; 22:0, behenic acid.

172 ^c "n.d.", not detected.

173 ^d "—", not calculated.

174 3.3. Effect of heat treatment of CG medium on fungal cultivation

175 When crude glycerol, as an inexpensive carbon source is used for a mass culture in a 176 bioreactor, a simpler sterilization method than autoclaving (121°C, 20 min) is desired. The 177 effect of heat treatment of the CG medium on fungal cultivation was examined. The growth 178 (indicated as DCW) of all strains was dependent on the temperature and time of heat 179 treatment, as shown in Fig. 2. Strains N1 and N3 did not grow at all in the CG medium 180 treated below 70°C, which indicated that the crude glycerol contains some growth 181 inhibitors (such as methanol) that are decomposed or converted on heat treatment. On the 182 other hand, growth of strain W1 was observed on cultivation in the CG medium treated 183 above 40°C (Fig. 2), which indicated that strain W1 has strong resistance to the toxicity of 184 the crude glycerol. The three strains were found to grow well in the CG medium treated at 185 105°C for one hour. The preparation of culture media is a challenge when mass culturing in 186 large culture devices. Preparing the medium by a simpler heat treatment rather than 187 autoclaving may lower the cost of culture. Crude glycerol, which contains alcohols, salts, 188 and heavy metals in addition to glycerol, is a byproduct of the chemical transesterification 189 of lipids in biodiesel production. The major impurity of methanol in the crude glycerol is 190 very toxic for microorganisms. The culture of these fungi in CG medium subjected to 191 simple heat treatment to produce microbial oils is expected to be new utilization method for 192 waste crude glycerol.



Fig. 2. Effect of heat treatment of the CG medium on fungal growth. *Penicillium* sp. N1
(A), *P. citrinum* N3 (B), and *F. oxysporum* W1 (C) were cultivated in CG medium
containing 4% crude glycerol for 7 days. The CG medium was heat-treated at 40, 50, 60, 70,
80, 90, 105, or 110°C for 30 min (dark grey) or 1 hour (light grey) before inoculation.

201 **4. Conclusion**

202 Utilization of crude glycerol is a serious issue in the process of generation of biodiesel. 203 Simple and efficient methods for its regeneration are required to avoid environmental 204 pollution. Three oleaginous fungi obtained in this study effectively produced biolipid in 205 medium containing waste crude glycerol. Two strains, Penicillium spp., isolated are 206 expected to be hosts accumulating FFAs. F. oxysporum W1 accumulated triacylglycerols as 207 a major lipid and grew well on medium containing crude glycerol only heat-treated without 208 autoclave sterilization. This study proposes a new application of crude glycerol to produce 209 microbial oils.

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211 CRediT authorship contribution statement

The authors' responsibilities were as follows: TS and ES conceived and designed the overall research. YK, CK, MK, and NM carried out the experimental work, analyzed, and interpreted data. TS and ES recommended and edited the paper. All authors contributed to the article and approved the submitted version.

216

217 **Declaration of competing interest**

218 The authors declare that there is no conflict of interest.

219

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227	Appendix A. Supplementary data
228	Supplementary material
229	
230	References
231	1. Ardi, M.S., Aroua, M.K., Awanis Hashim, N., 2015. Progress, prospect and challenges in
232	glycerol purification process: A review. Renew. Sust. Energ. Rev. 42, 1164-1173.
233	2. Chang, K.J.L., Paul, H., Nichols, P.D., 2015. Australian thraustochytrids: potential
234	production of dietary long-chain omega-3 oils using crude glycerol. J. Funct. Foods 19,
235	810-820.
236	3. Chatzifragkou, A., Papanikolaou, S., Dietz, D., Doulgeraki, A.I., Nychas, G.J.E., Zeng,
237	A.P., 2011. Production of 1, 3-propanediol by Clostridium butyricu growing on
238	biodiesel-derived crude glycerol through a non-sterilized fermentation process. Appl.
239	Microbiol. Biotechnol. 91, 101-112.
240	4. Chol, C.G., Dhabhai, R., Dalai, A.K., Reaney, M., 2018. Purification of crude glycerol
241	derived from biodiesel production process: experimental studies and techno-economic
242	analyses. Fuel Process. Technol. 178, 78-87.
243	5. Desbois, A.P., Smith, V.J., 2010. Antibacterial free fatty acids: activities, mechanisms of
244	action and biotechnological potential. Appl. Microbiol. Biotechnol. 85, 1629-1642.

245 6. Gao, Z., Ma, Y., Wang, Q., Zhang, M., Wang, J., Liu, Y., 2016. Effect of crude glycerol

- impurities on lipid preparation by *Rhodosporidium toruloides* yeast 32489. Bioresour.
 Technol. 218, 373-379.
- 248 7. Gutarra, M.L.E., Godoy, M.G., Maugeri, F., Rodrigues, M.I., Freire, D.M.G., Castilho,
- 249 L.R., 2009. Production of an acidic and thermostable lipase of the mesophilic fungus
- 250 *Penicillium simplicissimum* by solid-state fermentation. Bioresour. Technol. 100, 5249-5254.
- 8. Ilham, Z., Saka, S., 2016. Esterification of glycerol from biodiesel production to glycerol
- carbonate in non-catalytic supercritical dimethyl carbonate. Springerplus. 5 1.
- 9. Johnson, D.T., Taconi, K.A., 2007. The glycerin glut: options for the value-added
 conversion of crude glycerol resulting from biodiesel production. Environ. Prog. 26
 338-348.
- 10. Kumari, A., Ahmad, R., Negi, S., Khare, S.K., 2017. Biodegradation of waste grease by
 Penicillium chrysogenum for production of fatty acid. Bioresour. Technol. 226, 31-38.
- 258 11. Leoneti, A.B., Aragão-Leoneti, V., de Oliveira, S.V.W.B., 2012. Glycerol as a
- by-product of biodiesel production in Brazil: Alternatives for the use of unrefined glycerol.
- 260 Renewable Energy. 45, 138-145.
- 12. Liang, Y., Cui, Y., Trushenski, J., Blackburn, J. W., 2010. Converting crude glycerol
 derived from yellow grease to lipids through yeast fermentation. Bioresour. Technol. 101,
 7581-7586.
- 13. Lima, R.T., Alves, A.M., de Paula, A.V., de Castro, H.F., Andrade, G.S., 2019.
- 265 Mycelium-bound lipase from *Penicillium citrinum* as biocatalyst for the hydrolysis of
- 266 vegetable oils. Biocatal. Agric. Biotechnol. 22.
- 267 14. Maia, M.R.G., Chaudhary, L.C., Bestwick, C.S., Richardson, A.J., McKain, N., Larson,
- 268 T.R., Graham, I.A., Wallace, R.J., 2010. Toxicity of unsaturated fatty acids to the

- 269 biohydrogenating ruminal bacterium, *Butyrivibrio fibrisolvens*. BMC Microbiol. 10, 52.
- 270 15. Okuda, T., Ando, A., Negoro, H., Kikukawa, H., Sakamoto, T., Sakuradani, E., Shimizu,
- S., Ogawa, J., 2015. Omega-3 eicosatetraenoic acid production by molecular breeding of
- the mutant strain S14 derived from *Mortierella alpina* 1S-4. J. Biosci. Bioeng. 120,
- 273 299–304.
- 274 16. Polburee, P., Yongmanitchai, W., Lertwattanasakul, N., Ohashi, T., Fujiyama, K.,
- 275 Limtong, S., 2015. Characterization of oleaginous yeasts accumulating high levels of lipid
- when cultivated in glycerol and their potential for lipid production from biodiesel-derived
- 277 crude glycerol. Fungal Biol. 119, 1194-1204.
- 17. Poli, J.S., da Silva, M.A., Siqueira, E.P., Pasa, V.M., Rosa, C.A., Valente, P., 2014.
- 279 Microbial lipid produced by *Yarrowia lipolytica* QU21 using industrial waste: a potential
 280 feedstock for biodiesel production. Bioresour. Technol. 161, 320-326.
- 18. Tang, S., Boehme, L., Lam, H., Zhang, Z., 2009. *Pichia pastoris* fermentation for
 phytase production using crude glycerol from biodiesel production as the sole carbon
 source. Biochem. Eng. J. 43, 157-162.
- 19. Thompson, J.C., He, B.B., 2006. Characterization of crude glycerol from biodiesel
 production from multiple feedstocks. Appl. Eng. Agric. 22, 261-265.
- 286 20. Wan Isahak, W.N.R., Ramli, Z.A.C., Ismail, M., Jahim, L.M., Yarmo, M.A., 2015.
- 287 Recovery and purification of crude glycerol from vegetable oil transesterification. Sep.
- 288 Purif. Rev. 44, 250-267.
- 289 21. White, T.J., Bruns, T., Lee, S., Taylor, J.W., 1990. Amplification and direct sequencing
- 290 of fungal ribosomal RNA genes for phylogenetics, in: Innis, M.A., Gelfand D.H., Sninsky
- J.J., White T.J. (Eds.), PCR Meth Appl. San Diego: Academic Press, 315-322.



Supplemental Figure S1. Effect of glycerol concentrations on growth and lipid productivity. *Penicillium* sp. N1 (A), *P. citrinum* N3 (B), *Fusarium oxysporum* W1 (C), and *Mortierella alpina* CBS754.68 (D) as a standard strain of oleaginous filamentous fungi, were cultivated in the medium containing pure glycerol and 1% yeast extract for 7 days, at 28°C. Abbreviations: DCW, dry cell weight; TFA, total fatty acid.

Oleagingus granies	Crude glycerol component	Concentration of crude	Lipid yield	Lipid accumulation	Deferences	
Oleagillous species	(%) ^{a,b}	glycerol used (g/L) (% w/w)		Kelerences		
Penicillium sp. N1	Glycerol (45), Lipids ^c (13),	10% (w/v)	9.38	22.86	This study	
P. citrinum N3	MeOH (13), Salt (2.7)	10% (w/v)	4.93	16.80	This study	
Fusarium oxysporum W1		20% (w/v)	12.40	50.64	This study	
Rhodosporidium toruloides 32489	Glycerol (49), Oleate (2), MeOH (18), Salt (1)	4% (w/v)	6.20	41.76	(Gao et al., 2016)	
<i>R. fluviale</i> DMKU-RK253	Glycerol (82), NGOM (5.4), MeOH (0.1)	7% (w/v)	3.9	65.2	(Polburee et al., 2015)	
Aurantiochytrium sp. TC 20	Glycerol (41), Fat (0.08), MeOH (-°)	4% (w/v)	1.0	12.5	(Chang et al., 2015)	
Yarrowia lipolytica QU21	Glycerol (83), Lipids ^e (-), MeOH (0.008), Salt (5.2)	8.3% (w/v)	1.27	18.96	(Poli et al., 2014)	
Cryptococcus curvatus ATCC 20509	Glycerol (49), Lipids ^c (3), MeOH (23), Salt (-)	Total 437 g in 2 L fed-batch	17.4	52.9	(Liang et al., 2010)	

Supplemental Table S1. Crude glycerol composition used as a carbon source and yield and accumulation of biolipids.

^a The numbers in parenthesis indicate percentages.

^b Abbreviations: MeOH, methanol; NGOM, non-glycerol organics.

^c "Lipids" contains soaps, free fatty acids, and fatty acid methyl esters.

^d "-" indicates the components that were not described in the reference.